

# NOTATIONS

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# **NOTATION**

 $A_E = \%$  aromatics extracted

- a = interfacial area per unit volume of contactor,  $L^2/L^3$ ,  $L^{-1}$
- $a_t = surface area of packing per unit, L^2/L^3, L^{-1}$
- $d_v = packing size, L$
- d<sub>T</sub> =tower diameter, L
- d<sub>us</sub> = Sautermean diameter of droplets, L
- d<sub>us</sub><sup>o</sup> =characteristic droplet diameter, L
- D = diffusivity of solute,  $L^2T^{-1}$
- E = solubility of solute in the phase in which it is transferred,  $ML^{-3}$
- G =flow rate  $MT^{-1}L^{-2}$
- g = gravitational constant,  $LT^{-2}$
- $HTU^{-}$  = height of transfer unit, L
- $H_B$  = Concentration of solute in the extract phase expressed as gm. of solute per gm. of solvent in the extract phase.
- $H'_B$  = Concentration of solute in raffinate phase, expressed as gm. of solute per gm. of non-solute in the raffinate phase.
- $H_B^*$  = Equilibrium value of Concentration of solute in the extract phase expressed as gm. of solute per gm. of solvent in the extract phase.
- $H'_B^* =$  Equilibrium value of Concentration of solute in raffinate phase, expressed as gm. of solute per gm. of non-solute in the raffinate phase.

k<sub>c</sub>.=individual continuous phase mass transfer coefficient LT<sup>-1</sup>

- $k_d$  = individual dispersed phase mass transfer coefficient, LT<sup>-1</sup>
- k ' = Pseudo-first order reaction rate constant,  $T^{-1}$
- $K_L$  = mass transfer coefficient in the phase where reaction is taking place39,  $LT^{-1}$
- $K_{oca}$  = overall volumetric mass transfer coefficient based on continuous phase,  $T^{-1}$
- $K_{oda}$  = overall volumetric mass transfer coefficient based on dispersed phase, T<sup>-1</sup>
- L = ratio of dispersed phase to continuous phase velocities,  $V_d/V_c$
- m = slope of the equilibrium line
- N.T.U.= Number of transfer units
- NSc = Schemidt number,  $\mu/(p D)$
- %  $P_E$ =% purity of extract
- R = specific rate of extraction,  $ML^{-2}T^{-1}$
- $R_{cd}^{\dagger}$  = characteristic Reynolds number of dispersed phase



S/F=solvent to feed ratio, by wt. or by vol.

- V = superfacial velocity of the phase,  $LT^{-1}$ Vo = characteristic velocity,  $LT^{-1}$
- $V_s = slip velocity, LT^{-1}$
- $V_t$  = terminal velocity of liquid drops,  $LT^{-1}$
- W<sub>e</sub> = modified Weber number
- X = fractional hold-up of dispersed phase

# **GREEK LETTERS**

- O = contact time T
- $\gamma$  = interfacial tension, FL<sup>-1</sup>
- $\varepsilon$  = fractional voidage of column

 $\mu$  = viscosity, ML<sup>-1</sup> T<sup>-1</sup>

 $p = density, ML^{-3}$ 

 $\Delta p$  = density difference, ML<sup>-3</sup>

 $\sigma$  = surface tension, FL<sup>-1</sup>

σcr =critical surface tension

### **SUBSCRIPTS**

c = continuous phase

- d = dispersed phase
- f = flooding conditions

o = overall

s = fluid which does not wet the packing preferentially

w = fluid which preferentially wets the packing

1=based on Vd

2= based on Vd+Vc

### SPECIFIC NOTATIONS

#### Various constants

K, n = Constants in Hand's correlation.

 $K_c$ ,  $n_c = Constants$  in Campbell's correlation.

 $k_B \cdot {}^n_B$  = Constants in Batchman's correlation.

 $k_{0,T} \stackrel{n}{}_{0,T} = Constants in Othmer and Tobia$ 

#### (ii) Composition on Weight Basis :-

X HE =Wt. fraction of Hexane Extract

X HR = Wt. fraction of Hexane Raffinate

X SE = Wt. fraction of Solvent Extract X SR = Wt. fraction of Solvent Raffinate XBE =Wt. Fraction of Benzene in extract XBR=Wt. Fraction of Benzene in raffinate XD'E+WE=Wt. Fraction of Dmso+Water in extract XD'R+WR=Wt. Fraction of Dmso+Water in raffinate XD'E+WE= wt. fraction of dmso+water in extract XDE+WE=Wt. Fraction of Dmf+Water in extract XDR+WR=Wt. Fraction of Dmf+Water in raffinate XH'E=Wt. Fraction of Heptane in extract XH'R= wt. fraction of Heptane raffinate (iii) Flow rates in Packed column operation: Vci= continuous phase flow rate in let,  $LT^{-1}$ Vco= continuous phase flow rate out let,  $LT^{-1}$ Vdi= dispersed phase flow rate in let,  $LT^{-1}$ Vdo= dispersed phase flow rate out let,  $LT^{-1}$ Vcavg= Average continuous phase flow rate LT<sup>-1</sup> Vdavg g= Average dispersed phase flow rate  $LT^{-1}$ 

R.IE= Refractive Index Extract phase.

R.IR= Refractive Index raffinate. phase.

#### (iv) For Packed column internals.

I.D=. inside diameter of Packing cm

O.D=. out side diameter of Packing cm

L = Length of one Packing. cm

dp = diameter of Packing . cm

dc= diameter of column cm

# (v) Abbreviations for Chemicals

A= aromatics

Dmf = dimethyl formamide

Dmso = dimethyl sulfoxide

DEG = diethylene glycol

TEG = triethylene glycol

H-Hexane, T=Toluene X=Xylene

H'=Heptane, O=Octane,